

WeCo

metTop



COMBINED COMPETENCE UNDER ONE ROOF

METTOP

- Tankhouse Technology



PIERER
Konzern
gesellschaft mbH

Pierer
Konzerngesellschaft AG
gets part of the company

Patent registration
METTOP-BRX
Technology for
tankhouse optimization

Patent registration ILTEC
Technology for water free
cooling

2007

2009

2015

2005

2014

2018

2019

Founding of Mettop by
Iris and Andreas
Filzwieser and Stefan
Wallner

Founding of
UrbanGold for
Copper
Recycling

First industrial
scale plant for E-
waste recycling

Mettop becomes
shareholder of Welding
Copper in Spain

UrbanGold
recycling for a green future

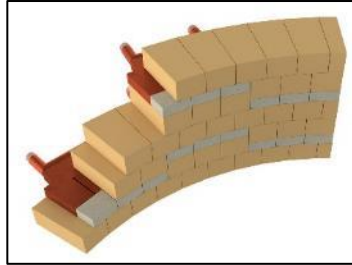
Overview Products and Services



Non-ferrous metals units

Products:

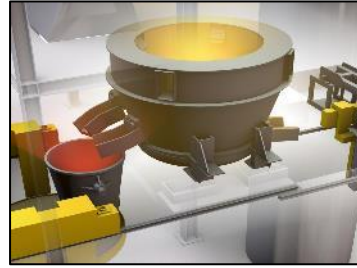
- ◆ HENRI[®]
- ◆ Gas Purging Systems
- ◆ CFM Coolers
- ◆ ionicLife cast



Refractories non-ferrous

Products:

- ◆ 3D Engineering + supply
- ◆ CFD modeling
- ◆ HT-calculations
- ◆ EXP-calculations



E-waste recycling UrbanGold

Products:

- ◆ Process Engineering
 - ◆ UG Compact
 - ◆ UG Flex
 - ◆ UG Classic
- ◆ Market Studies



Tankhouse technology

Products:

- ◆ METTOP-BRX[®] Technology
- ◆ Cathode spacers
- ◆ Complete Tankhouse



ILTEC for vessel cooling

Products:

- ◆ IL-B2001[®]
- ◆ Ionic Liquid Technology for vessel cooling
- ◆ Furnace integrity optimization

Overall Process & Technology Consulting

Field Studies & Trainings

Process and 3D Plant Engineering



Research & Development & Innovation

DigMet





melTop

METTOP-BRX Technology

New Approach to Higher Current Densities and Higher Productivity

Tankhouse Solutions

More than 400 A/m² –
yesterday an illusion, today reality

Innovative technology to us means considering new directions and adopting unconventional approaches to maximize productivity and quality.

In order to increase the productivity of a copper tankhouse, the current efficiency and/or current density have to be increased..



Available systems for refining and winning electrolysis

Conventional Refining Electrolysis

Copper cathodes
MOTHERSHEETS

max. 300 A/m²



Conventional Refining Electrolysis

Copper cathodes
STAINLESS STEEL

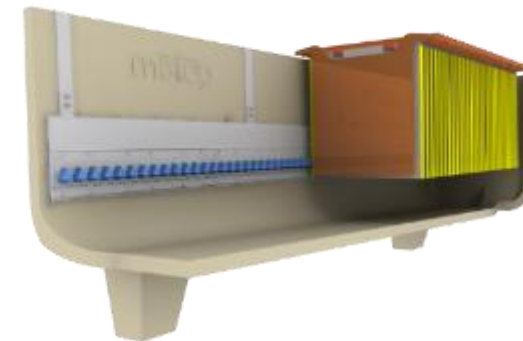
max. 350 A/m²



METTOP-BRX Refining Electrolysis

Mothersheets or
stainless steel

max. 450 A/m²



Meet customers' problems – considerations to choose METTOP-BRX Technology

Targets for Tankhouse optimization:

- High current efficiency
- High chemical cathode quality
- Low operating cost
- Lower footprint
- Low bound capital

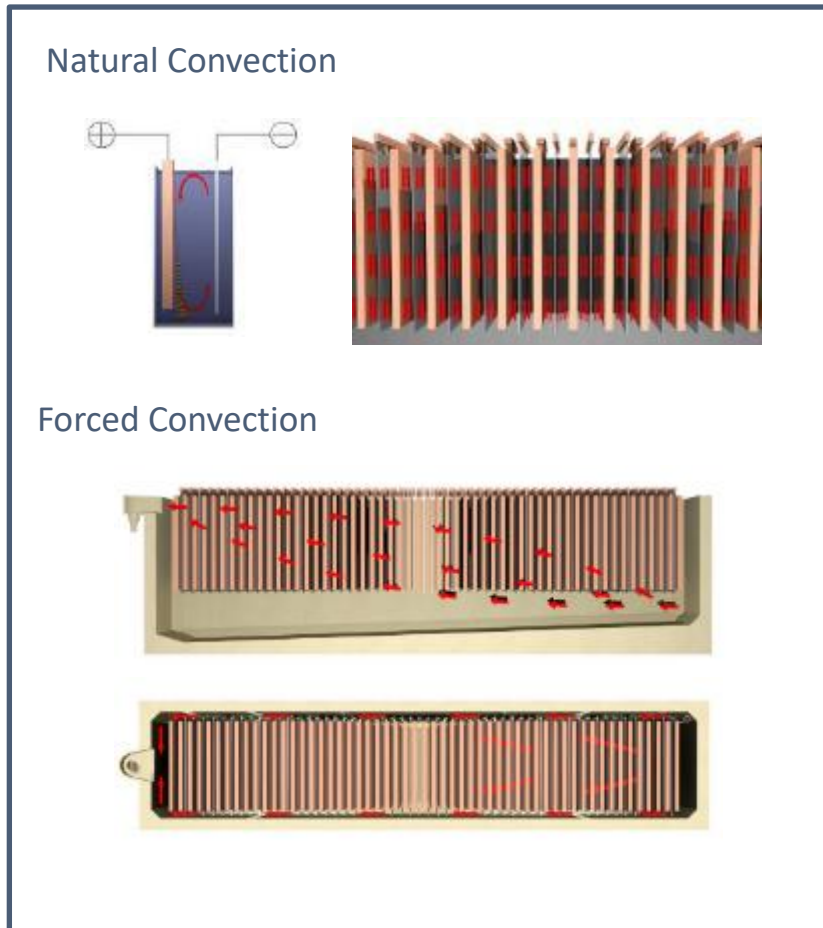
METTOP-BRX Technology enables **higher current densities** and will result in **higher productivity**.

Examples of applications:

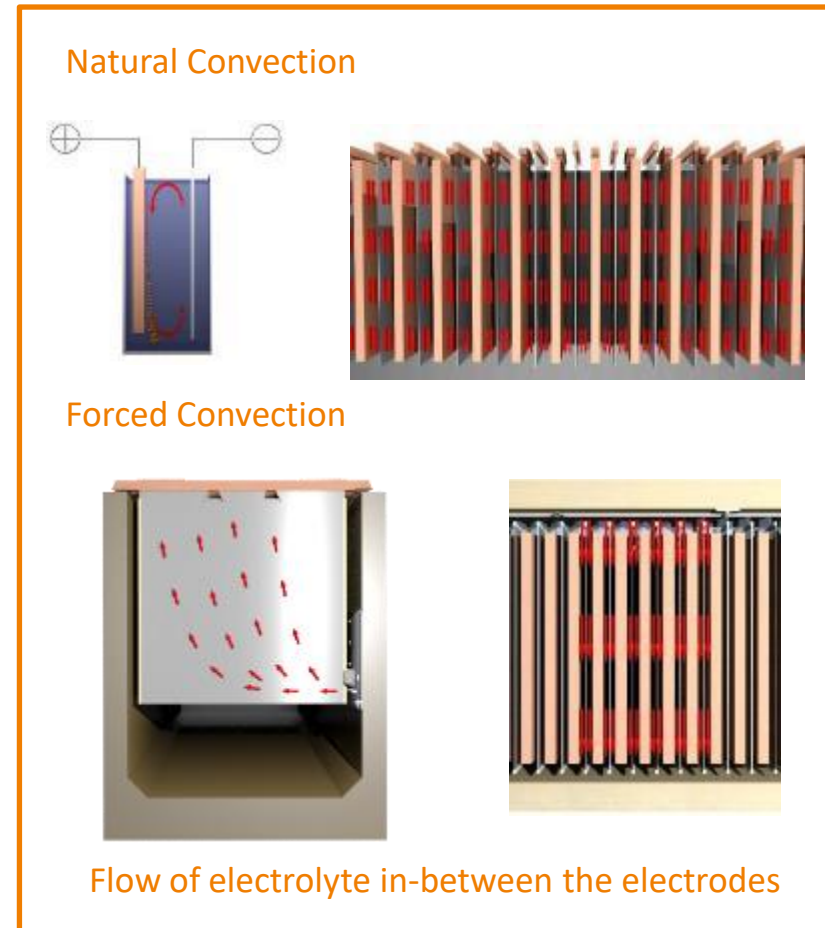
- Refining and winning electrolysis for copper
- Electrolysis for zinc
- Tankhouses for descaling

Different flow mechanisms and improvement by METTOP-BRX Technology

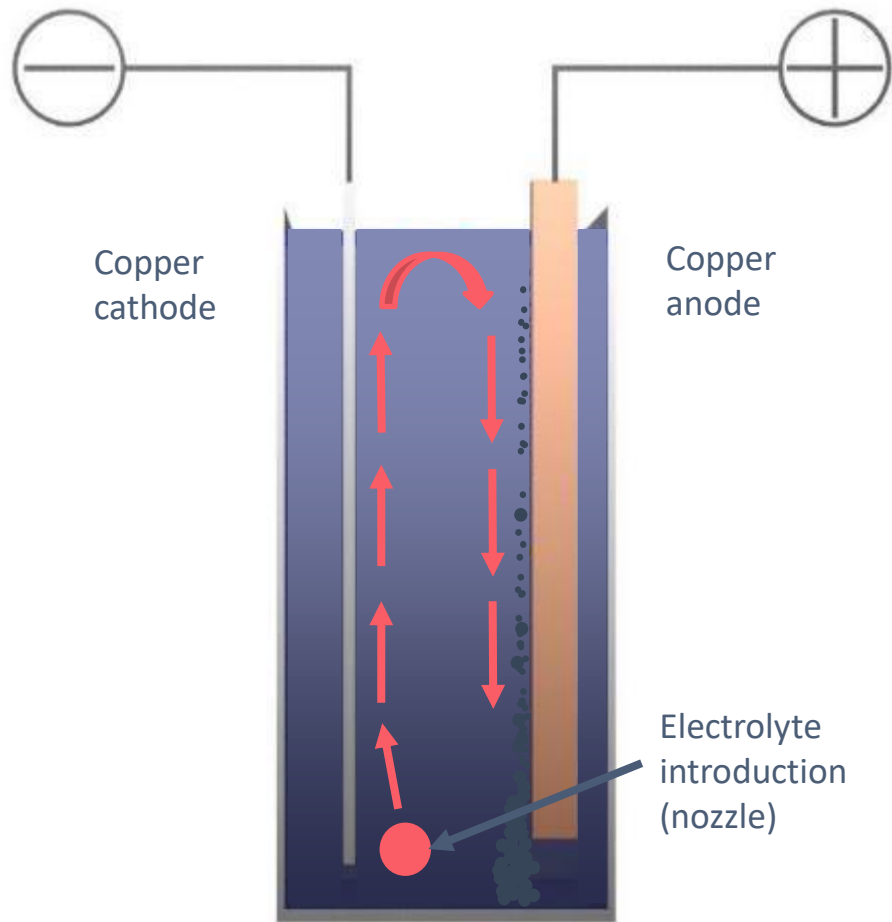
Conventional



METTOP-BRX Technology



More homogeneous conditions and no influence of anode slime

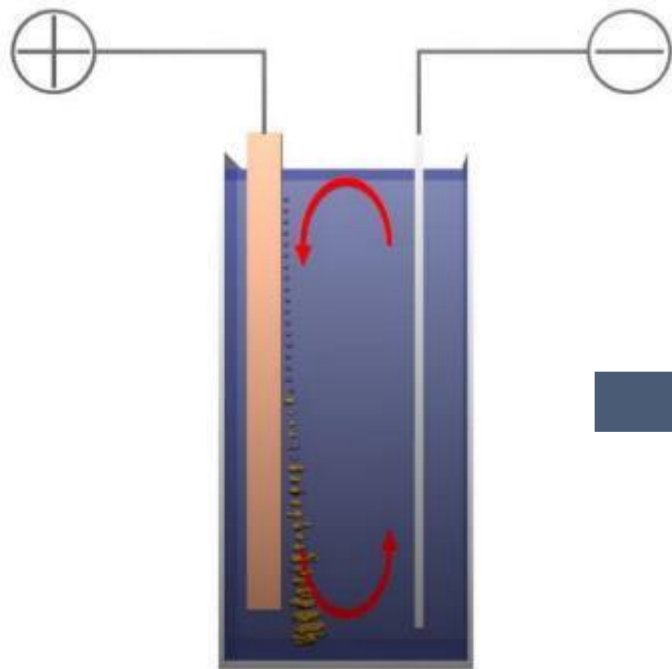


Improvements:

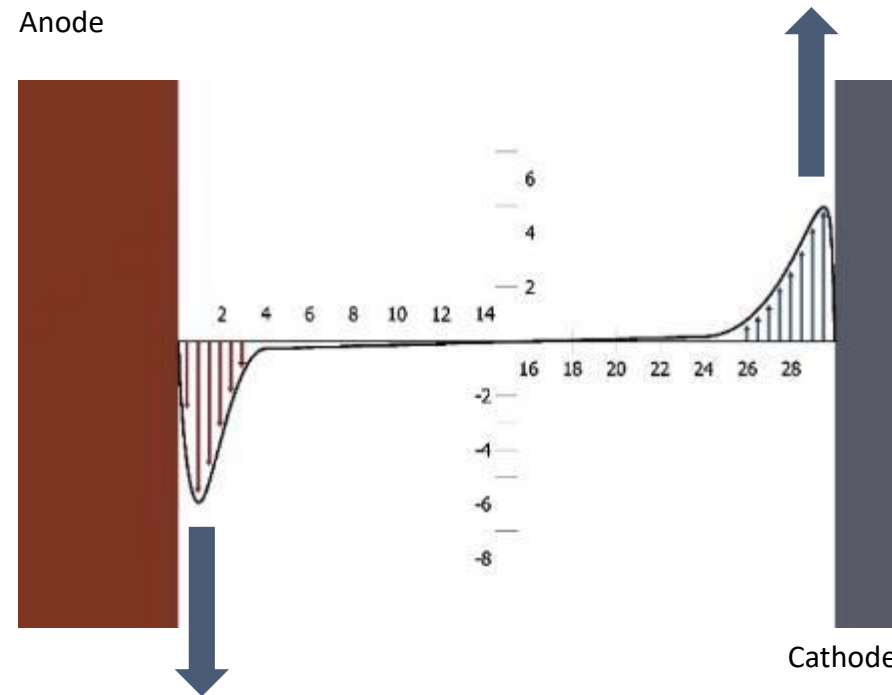
- Introduction of the electrolyte near the active cathode surface -> **direct injection of the inhibitor** near the surface -> increasing quality of the cathodes
- More **homogeneous temperature** distribution
- No influence of **anode slime settlement** because of enhancement of the already existing flow, resulting from natural convection

What is different? - Improvement flow mechanism by Mettop's BRX Technology

Natural Convection

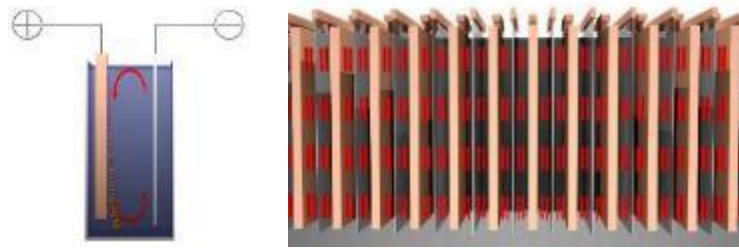


Natural & Forced Convection

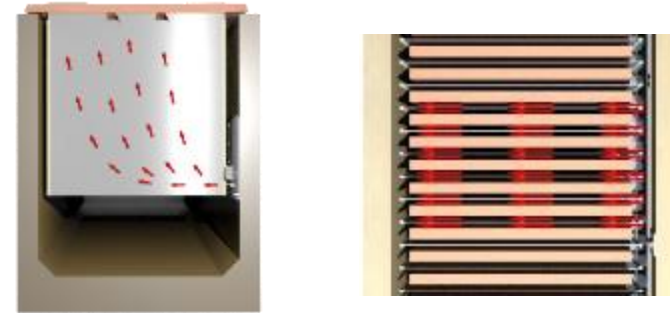


What is different? - Improvement flow mechanism by Mettop's BRX Technology

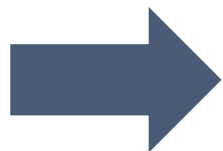
Enhanced Natural Convection



Forced Convection



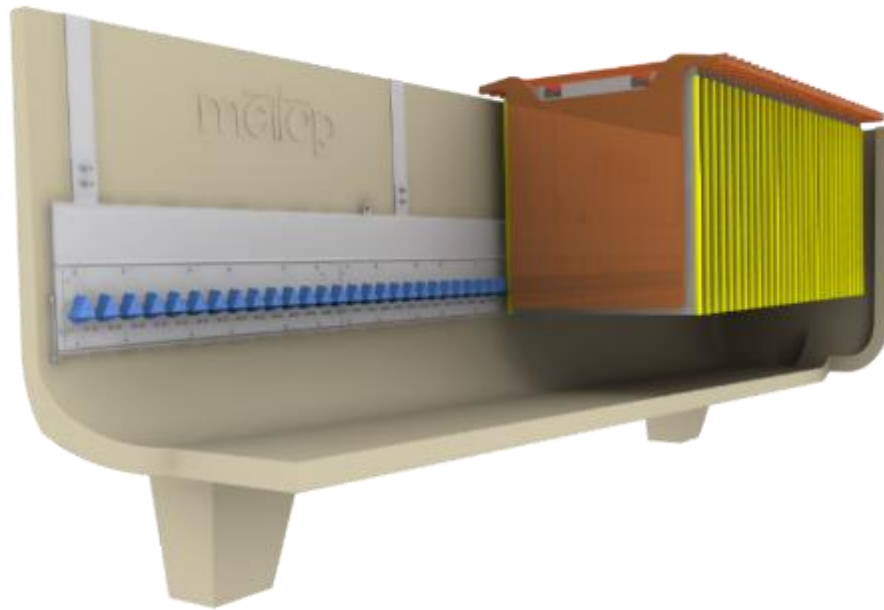
- Higher electrolyte flow rate and flow directly in front of the cathode leads to a **decreased diffusion boundary** layer.
- Direct introduction of the inhibitors near the active cathode surface lead to a more **homogeneous distribution**
- Current density distributions is more homogenous
- Direct electrolyte introduction leads to a more homogenous electrolyte temperature distribution



Using the METTOP-BRX Technology a current density of up to **450 A/m²** at a **current efficiency of above 98 %** can be achieved.

Can Mettop's BRX Technology be realized in existing Tankhouses?

Brownfield Approach – Parallel Flow Device (PFD) for upgrading existing tankhouses



- Special positioning devices – **cathode spacers** for accurate electrode positioning
- PFDs are customer-tailored to guarantee optimum results for each specific tankhouse.

Is Mettop's BRX Technology a proven Technology?

Montanwerke Brixlegg AG, Austria – Upscaling an Existing Tankhouse in 2007



- Higher **current density** and **increased production**
- Additive adjustments for **current efficiency increase**
- Better **cathode quality** due to more homogeneous additive distribution
- **Shorter down times** when filling the groups due to higher flow and faster filling
- Higher flow for **faster heating-up** of the anodes
- **Fewer shorts occur** due to accurate cathode positioning/guiding system.



祥光铜业
XIANGGUANG COPPER

Is Mettop's BRX Technology a proven Technology?

Xiangguang Copper, China – Installation of a new Tankhouse in 2011



- Pumps for **direct pumping** (i.e., no overhead tanks) for approximately 100 l/min per cell
- New design of electrical system for 420 A/m² (2 electric circuits) and new design of heat exchangers
- Continuous addition of inhibitors
- **Increase in productivity** from 200 000 t/year (conventional cell) to 300 000 t/year (METTOP-BRX)



Xiangguang Copper reports current efficiency of > 99 % at 420 A/m²

Standard tankhouse

Tankhouse1 Standard

| Year | 2012 | 2013 | 2014 | 2015 | 2016 | 2017 | 2018 | 2019 | 2020 | 2021 |
|-----------------------------------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|
| Current density, A/m ² | 265 | 265 | 265 | 265 | 294 | 294 | 294 | 265 | 265 | 265 |
| Current efficiency, % | 97,66 | 97,74 | 97,71 | 97,65 | 97,44 | 98,2 | 98,74 | 98,67 | 98,79 | 98,76 |
| Production, t | 152452 | 168494 | 202470 | 138263 | 197865 | 188468 | 217468 | 179765 | 178042 | 138085 |
| Scrap rate, % | 15,68 | 15,55 | 15,25 | 15,69 | 15,55 | 14,96 | 14,25 | 12,57 | 13,06 | 12,71 |
| DC power consumption, kWh/t | 278,28 | 282,41 | 271,41 | 291,39 | 290,72 | 295,2 | 299,06 | 285,76 | 279,52 | 290,142 |
| Amount of steam, t | 67568 | 67111 | 82203 | 63508 | 88558 | 82599 | 99511 | 85128 | 88291 | 68230 |
| Cu in cathode, % | 99,9976 | 99,9977 | 99,9976 | 99,9977 | 99,9978 | 99,9977 | 99,9978 | 99,9977 | 99,9977 | 99,9976 |
| No. of workers | 130 | 130 | 130 | 130 | 130 | 103 | 103 | 103 | 103 | 103 |
| Cathode quantity, (in% LME A) | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 |
| Ag in cathode, % | 0,000915 | 0,000955 | 0,000889 | 0,000812 | 0,000823 | 0,000954 | 0,000948 | 0,000899 | 0,000969 | 0,001046 |

Average

| |
|-------------------------------|
| 273,70 A/m² |
| 98,14 % |
| 176137,20 t |
| 14,53 % |
| 286,39 kWh/t |
| 45,00 kg/t |
| 99,998 % |
| 100,00 |
| 9,21 ppm |

Mettop Technology

Tankhouse 2 METTOP

| Year | 2012 | 2013 | 2014 | 2015 | 2016 | 2017 | 2018 | 2019 | 2020 | 2021 |
|-----------------------------------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|
| Current density, A/m ² | 410 | 410 | 410 | 385 | 385 | 410 | 410 | 385 | 385 | 385 |
| Current efficiency, % | 99,17 | 99,19 | 99,25 | 99,2 | 99,22 | 99,31 | 99,21 | 99,28 | 99,21 | 99,19 |
| Production, t | 271580 | 265258 | 282285 | 252859 | 245415 | 262972 | 244838 | 283211 | 263247 | 201528 |
| Scrap rate, % | 13,2 | 13,25 | 13,17 | 13,22 | 13,18 | 13,13 | 12,57 | 12,44 | 12,51 | 12,74 |
| DC power consumption, kWh/t | 361 | 359 | 362 | 359 | 353 | 363 | 377 | 355 | 358 | 362 |
| Amount of steam, t | 3658 | 4103 | 4430 | 4132 | 4322 | 4102 | 3906 | 4519 | 4106 | 3785 |
| Cu in cathode, % | 99,998 | 99,998 | 99,9979 | 99,9978 | 99,9978 | 99,9979 | 99,9979 | 99,9977 | 99,9977 | 99,9977 |
| No. of workers | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 |
| Cathode quantity, (in% LME A) | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 | 100 |
| Ag in cathode, % | 0,000486 | 0,000513 | 0,000498 | 0,000568 | 0,000589 | 0,000445 | 0,000425 | 0,000434 | 0,000389 | 0,000468 |

| |
|------------------------------|
| Average |
| 397,5 A/m² |
| 99,223 % |
| 257319,3 t |
| 12,941 % |
| 360,9 kWh/t |
| 1,6 kg/t |
| 100,00 % |
| 100 |
| 100 |
| 4,82 ppm |

Standard vs Mettop

| | Standard | Mettop |
|-------------------------------|------------------------|------------------------------|
| Current density | 273,7 A/m ² | 397,5 A/m² |
| Current efficiency | 98,1 % | 99,2 % |
| Production | 176137,2 t | 257319,3 t |
| Scrap rate | 14,5 % | 12,9 % |
| DC power consumption, kWh/t | 286,4 kWh/t | 360,9 kWh/t |
| Amount of steam | 45 kg/t | 1,6 kg/t |
| Cu in cathode, % | 99,998 % | 99,998 % |
| No. of workers | 103 | 100 |
| Cathode quantity, (in% LME A) | 100 | 100 |
| Ag in cathode | 9,2 ppm | 4,8 ppm |

Official statements XG

**STATEMENT
For
PARALLEL FLOW TECHNOLOGY APPLICATION**

Sep 12, 2020

Xiangguang Copper started the copper smelter construction in 2005 and the smelter was put into production in 2007. The Phase 1st tankhouse has a capacity of 200k tons, adopting conventional permanent stainless steel cathode electrolysis technology (720 cells). The smelting capacity of Xiangguang Copper was increased to 500k tons in 2011. To meet up with the smelting capacity, Xiangguang Copper cooperated with Mettop in its Phase 2nd tankhouse, adopting the new parallel flow technology in all the 720 cells. Thanks to the higher current density, the Phase 2nd tankhouse capacity reached 300k tons. The total electrolysis capacity (Phase 1st+Phase 2nd) reached 500k tons.

The Phase 2nd tankhouse of Xiangguang was put into production in June, the current density reached the 385A/m² in July and 420A/m² in October in 2011, every indicator is excellent and the production has been very stable up to now. Comparing to the conventional electrolysis technology adopted in Phase 1st, the parallel flow technology has the following advantages:

- Higher capacity

The operation current density of Phase 2nd tankhouse of Xiangguang is 420A/m² and that of the Phase 1st tankhouse is 280A/m². With the same number of cells, the capacity is increased by 50%.
- Lower investment

Comparing to conventional electrolysis technology, the investment of civil construction of Parallel Flow technology is lower, saving about 17%.
- Shorter anode life and lower fund occupation

With Parallel technology, the anode life is shortened from 20 days to 15 days and the anodes stored in the cells are less, thus the fund occupation of copper, gold and silver

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Tel: +86 635 713 5054

is lower.

- Improved copper quality

The copper content of cathode copper maintains above 99.9975% and is in accordance with high purity cathode copper standard. The quality of cathode copper is better than that of conventional permanent stainless steel cathode electrolysis technology.
- Higher silver reclaim rate

The silver content in the Phase 2 tankhouse cathode copper is less than 5ppm, while it is about 10ppm in Phase 1st tankhouse cathode copper. The silver reclaim rate is also higher.
- Higher current efficiency and lower comprehensive energy consumption

The current efficiency of Phase 2nd tankhouse is about 99.4%, while it is 97.5% for Phase 1st tankhouse. In addition, steam is not necessary for heating up in Phase 2nd tankhouse. The comprehensive energy consumption in Phase 2nd tankhouse is about 25% lower than that of Phase 1st tankhouse.

Zhou Songlin

Vice President

Yanggu Xiangguang Copper Co., Ltd

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Main Performance Figures for PF Electrolysis Technology of Xiangguang Copper

Sep 18th, 2020

The following are the main production performance figures of Xiangguang Copper from Jan 2019 to Aug 2020:

| Item No. | Description | Unit | Figures |
|----------|----------------------------------|------------------|-----------|
| 1 | No. of Cells | pc | 720 |
| 2 | Output of cathodes | kt | 470.14 |
| 3 | Recovery of copper | % | 99.7 |
| 4 | Current density | A/m ² | 385 |
| 5 | Anode life | d | 16 |
| 6 | Cathode life | d | 5/5/6 |
| 7 | Rate of scrap | % | 12.5 |
| 8 | Cell voltage | V | 0.32-0.50 |
| 9 | Current efficiency | % | 99.27 |
| 10 | Cell utilization rate | % | 93 |
| 11 | Electrolyte circulating velocity | L/min | 80-150 |
| 12 | Steam consumption | t/t·Cu | 0 |
| 13 | Ac Power consumption | KWH/t·Cu | 450 |
| 14 | Complementary energy consumption | Kgce/ t·Cu | 55.31 |

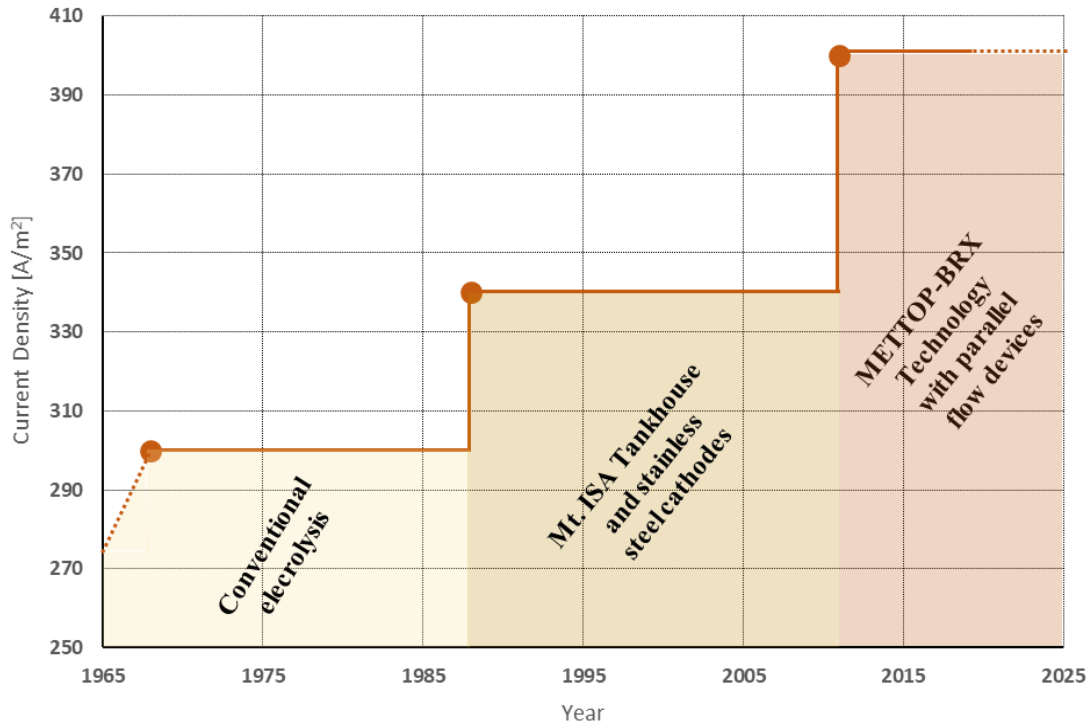
Zhou Songlin

Vice President

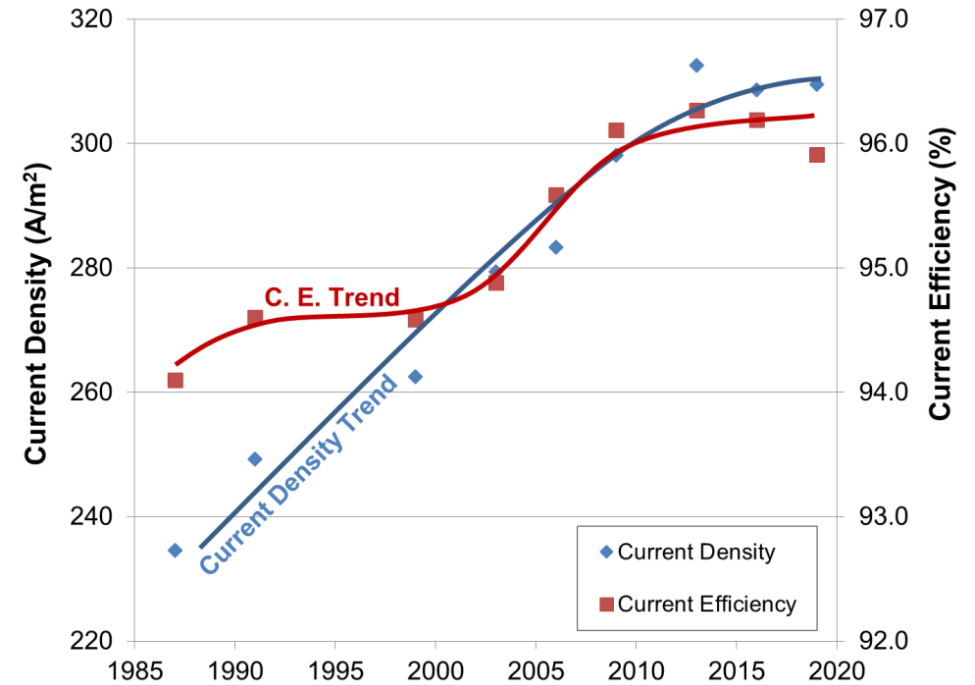
Yanggu Xiangguang Copper Co., Ltd

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Tel: +86 635 713 5054

Comparison of current density – historical background



Milestones for electrolysis and increase in current density
(Source: Filzwieser, et al., 2009, Filzwieser et al., 2014)



Average current density and current efficiency (C.E.) from 1987 to 2016
Source: GLOBAL SURVEY OF COPPER ELECTROREFINING: 2019 WORLD TANKHOUSE OPERATING DATA; Michael S. Moats [2019]

| Average current density (according to Davenport 2019) | Maximum current density ISA Technology | METTOP-BRX Technology |
|----------------------------------------------------------|-------------------------------------------|--------------------------|
| 300 A/m ² | 330-350 A/m ² | 380-420 A/m ² |

Summary

Today's most advanced tankhouse technology – the METTOP-BRX Technology – allows:

- Increasing the **current density and productivity** by up to 50 % compared to conventional copper electrorefining tankhouses.
- Can either be installed in **existing facilities** – in order to increase production – or considered in **new plants** – in order to reduce the footprint of the entire tankhouse.
- Right now the **benchmark** for a copper refinery is Xiangguang Copper, China, running their tankhouse no. 2 at 420 A/m² at a current efficiency > 99 % using the METTOP-BRX Technology.



melTop

Cathode Spacers

Immediately increase your current efficiency up to 2-3%

COMBINED COMPETENCE UNDER ONE ROOF

DigMet

Cell voltage monitoring system

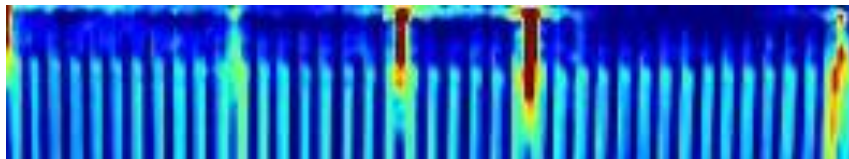


Automatic Detection

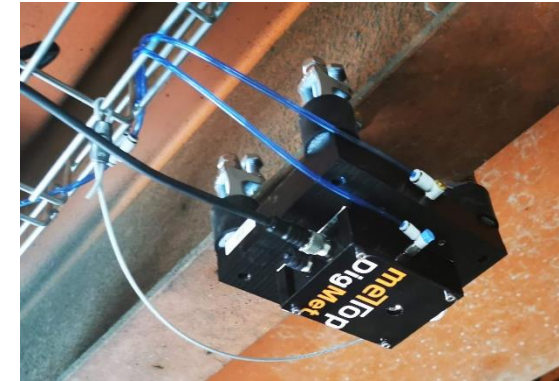
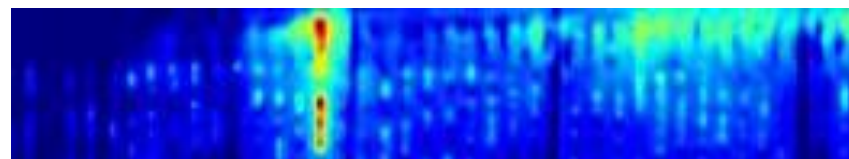
Detection with thermal cameras

- Optimized for short-circuit detection
- Sulfuric acid resistant housing
- Detection despite cell cover

No cover



With cover



Benefit of automatic detection

Savings potential

- Higher current efficiency
- Lower reworking costs

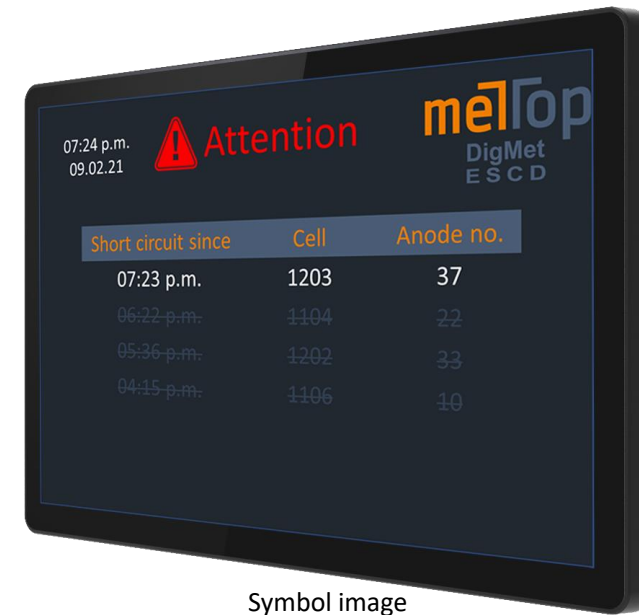
Minimization of the short circuit time from 12 hours to less than 2 hours

With increase of the current yield by 1% and annual production of 100,000 t a saving potential of 250,000 € results

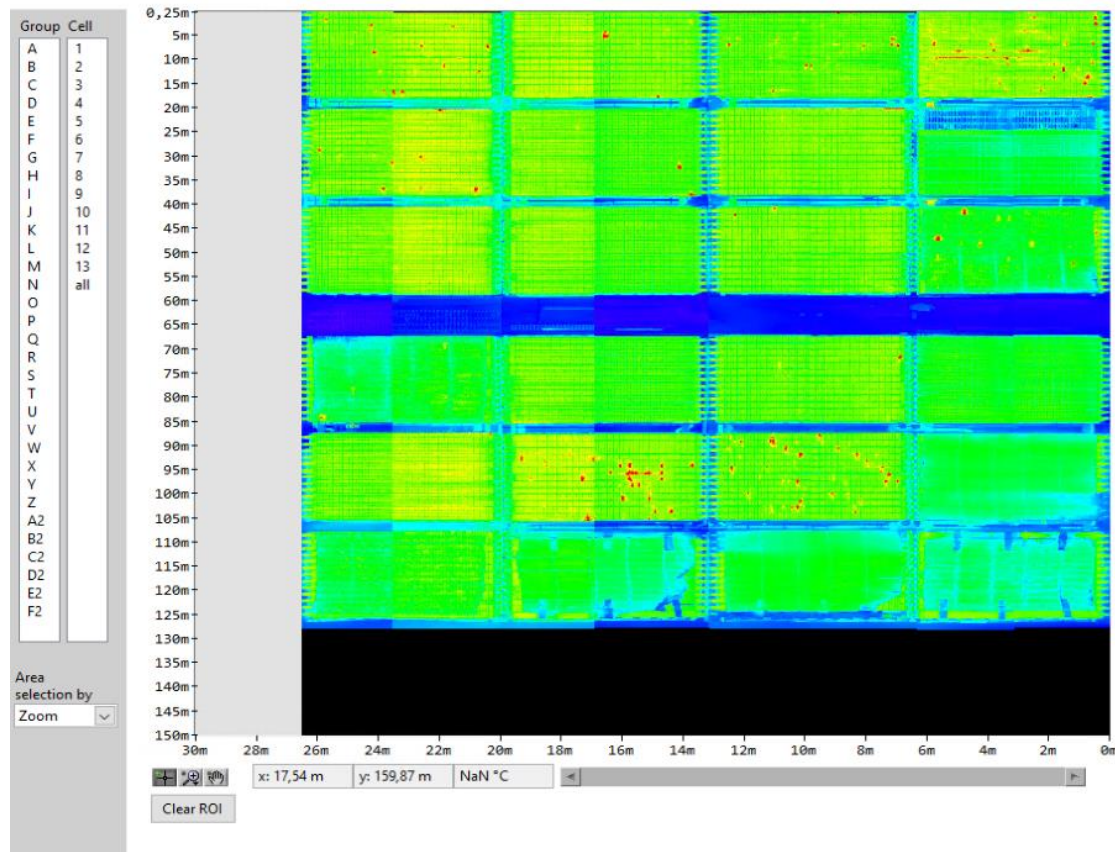
Automatic Detection

Display of short circuits in the tankhouse

- Shock resistant displays
- Variable screen size
- Acid resistant
- IP65 certified

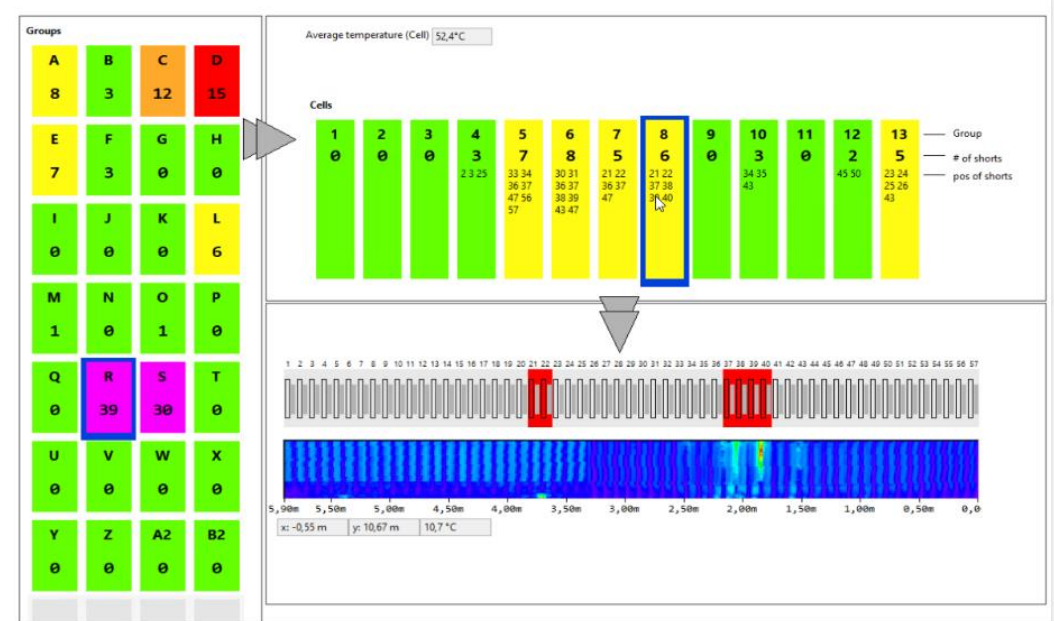


DigMet-Software



Symbol image

- Visualization of the tankhouse
 - With all groups and cells
 - Display of highly affected groups
 - Number of short circuits per group and cell



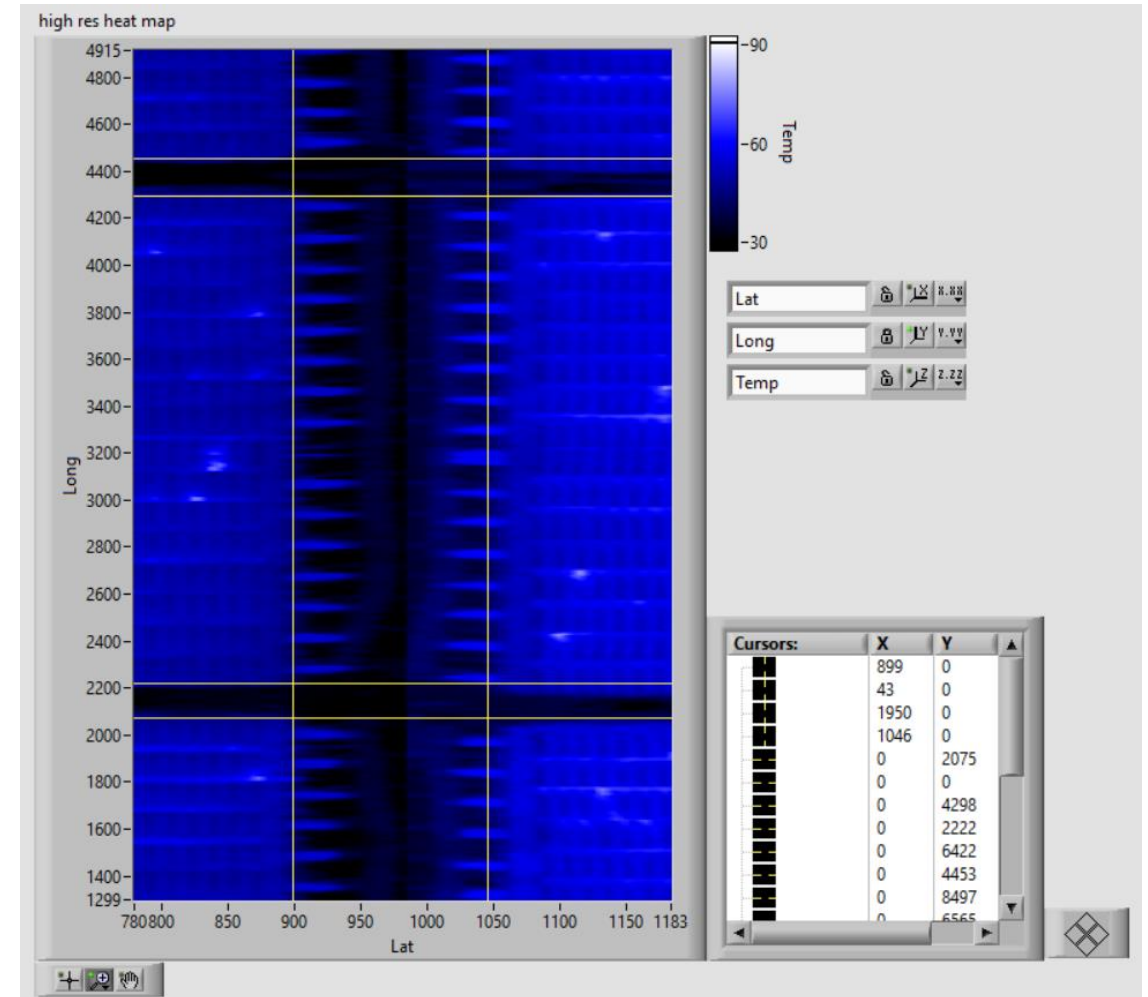
DigMet-Software

- Export and Visualization of
 - Short-circuits
 - Anode/Cathode temperatures
 - Busbar temperature
 - Electrolyte outlet temperature

| Pos | Max | AVG | AVG_Dev | Pos | Max | AVG | AVG_Dev | Pos | Max | AVG | AVG_Dev | Pos |
|----------|--------|--------|---------|----------|--------|--------|---------|---------|---------|--------|---------|---------|
| A2_05_57 | 57,1°C | 47,8°C | 6,1°C | B2_01_08 | 64,8°C | 49,1°C | 8,7°C | B_01_02 | 83,2°C | 59,7°C | 7,7°C | H_13_14 |
| A2_07_57 | 55,5°C | 47,8°C | 7,0°C | B2_01_33 | 65,2°C | 46,8°C | 6,5°C | B_02_23 | 79,1°C | 58,3°C | 5,6°C | H_11_56 |
| A2_08_57 | 57,1°C | 49,9°C | 9,9°C | B2_01_34 | 62,7°C | 46,0°C | 5,6°C | D_01_37 | 65,4°C | 54,4°C | 6,1°C | L_03_32 |
| A2_09_57 | 55,8°C | 51,3°C | 10,9°C | B2_01_54 | 54,4°C | 46,3°C | 5,9°C | D_03_32 | 77,4°C | 57,5°C | 6,8°C | K_06_57 |
| A2_10_57 | 56,3°C | 48,8°C | 7,7°C | B2_01_57 | 52,5°C | 46,2°C | 5,8°C | D_07_01 | 109,4°C | 58,7°C | 7,8°C | K_06_57 |
| A2_11_57 | 56,8°C | 50,3°C | 9,3°C | B2_02_11 | 66,7°C | 46,2°C | 5,9°C | D_11_55 | 80,6°C | 56,3°C | 6,0°C | L_01_57 |
| A2_12_57 | 55,0°C | 49,2°C | 8,5°C | B2_02_55 | 54,6°C | 46,0°C | 5,7°C | E_01_57 | 66,7°C | 52,5°C | 6,1°C | L_02_57 |
| A_01_16 | 71,4°C | 53,5°C | 6,0°C | B2_02_57 | 52,9°C | 46,9°C | 6,6°C | E_05_02 | 89,0°C | 52,8°C | 6,5°C | L_03_32 |
| A_04_25 | 80,3°C | 58,4°C | 10,7°C | B2_03_55 | 54,6°C | 46,5°C | 5,3°C | E_11_57 | 58,4°C | 51,2°C | 5,2°C | M_01_57 |
| A_05_16 | 68,1°C | 53,5°C | 6,3°C | B2_03_57 | 53,5°C | 46,6°C | 5,4°C | G_01_24 | 85,1°C | 58,4°C | 7,1°C | M_01_57 |
| A_05_24 | 82,5°C | 54,5°C | 7,3°C | B2_04_32 | 72,0°C | 49,8°C | 7,2°C | G_04_31 | 75,9°C | 57,0°C | 5,7°C | M_01_57 |
| A_05_36 | 67,2°C | 52,3°C | 5,1°C | B2_04_55 | 55,7°C | 48,0°C | 5,5°C | G_10_52 | 70,2°C | 58,3°C | 6,8°C | M_01_57 |
| A_06_49 | 78,1°C | 54,7°C | 8,2°C | B2_06_56 | 55,0°C | 46,8°C | 5,2°C | G_10_53 | 95,5°C | 63,6°C | 12,1°C | M_01_57 |
| A_06_50 | 78,1°C | 53,8°C | 7,3°C | B2_07_57 | 54,2°C | 46,3°C | 6,2°C | H_02_25 | 83,3°C | 60,9°C | 10,5°C | M_01_57 |
| A_07_21 | 76,0°C | 53,6°C | 6,8°C | B2_09_57 | 54,4°C | 48,0°C | 8,2°C | H_02_26 | 82,5°C | 57,0°C | 6,7°C | M_01_57 |
| A_10_15 | 68,7°C | 51,8°C | 5,7°C | B2_10_26 | 70,8°C | 48,1°C | 8,7°C | H_07_45 | 71,2°C | 53,9°C | 5,8°C | M_01_57 |
| A_12_20 | 66,1°C | 52,0°C | 5,8°C | B2_11_20 | 71,1°C | 46,6°C | 7,1°C | H_10_52 | 84,7°C | 53,9°C | 6,5°C | M_01_57 |
| A_13_38 | 62,2°C | 49,2°C | 5,7°C | B2_11_21 | 75,5°C | 50,1°C | 10,6°C | H_11_40 | 78,7°C | 57,5°C | 10,5°C | M_01_57 |
| A_13_47 | 64,8°C | 51,1°C | 7,6°C | B2_11_52 | 63,6°C | 46,9°C | 7,4°C | H_11_56 | 59,1°C | 52,1°C | 5,1°C | M_01_57 |
| B2_01_07 | 71,4°C | 49,8°C | 9,4°C | B2_11_57 | 54,1°C | 47,7°C | 8,2°C | H_13_14 | 84,4°C | 52,2°C | 6,1°C | M_01_57 |

DigMet-Software

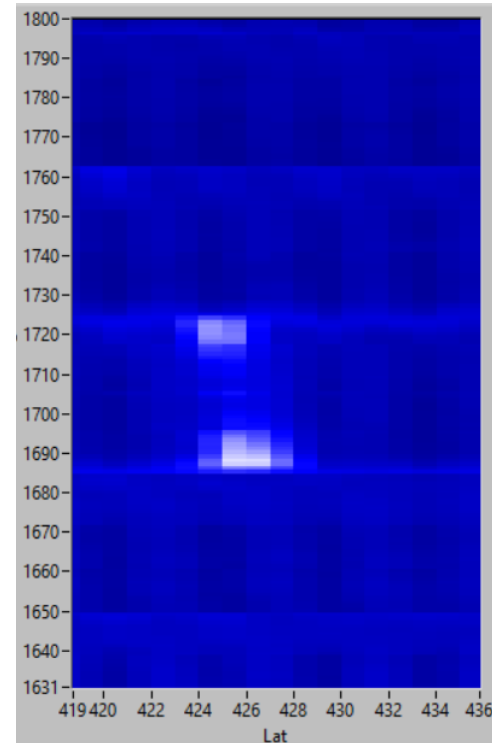
- Advanced Cell Detection
 - Automatic calibration
 - For easy calibration of the system
 - In the case of a camera exchange, the calibration is omitted
 - No need of crane positioning system



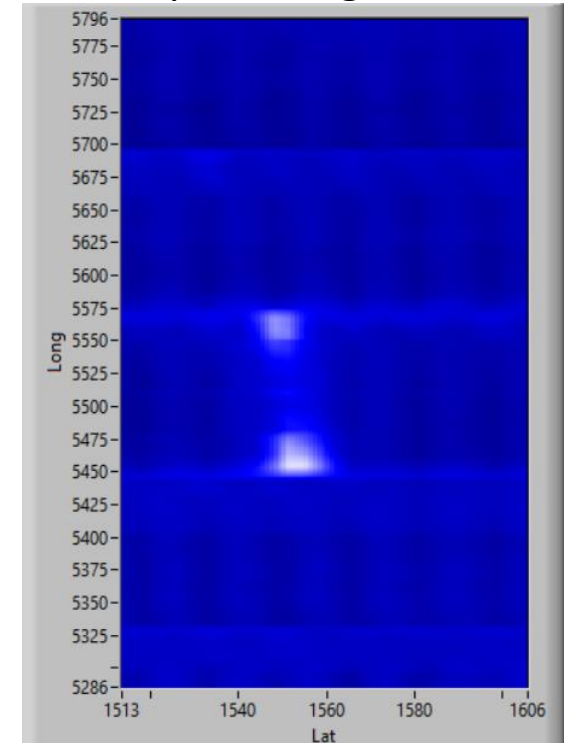
DigMet-Software

- Innovative Image Resampling Technology
 - Better short-circuit detection
 - More precise position
 - Accuracy of up to ± 0 anodes/cathodes

Standard thermal image



Resampled Image

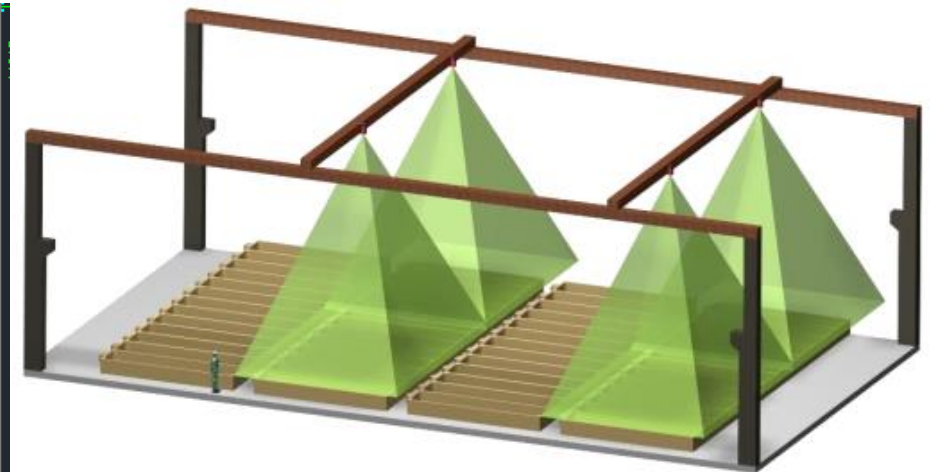
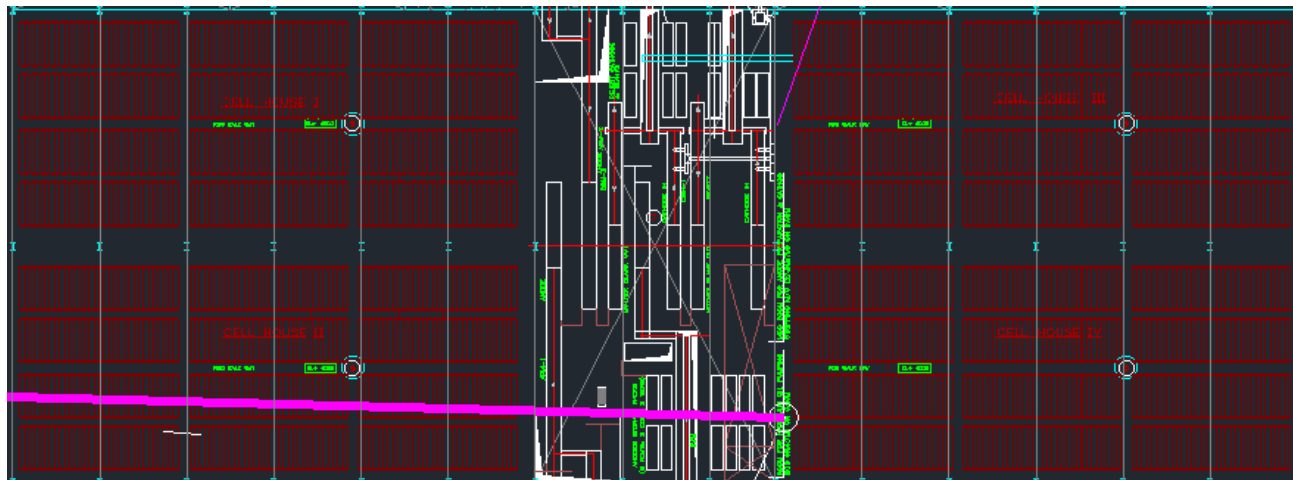


Mounting options

- Fixed cameras
- Crane
- Sliding rail
- ...

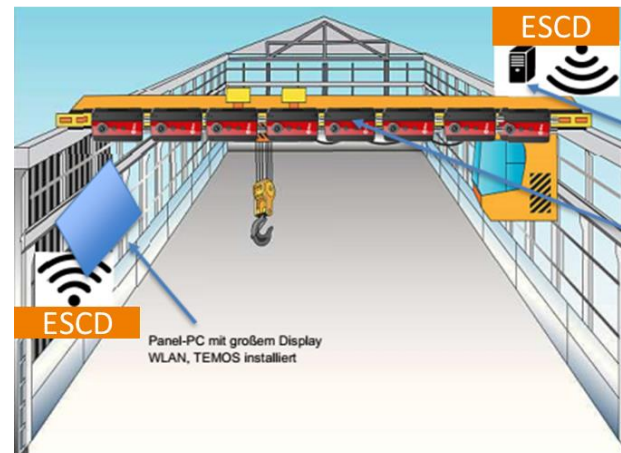
Fixed cameras

- Permanent monitoring
 - Independent of the crane
 - Fast response times
- Cameras needed:
 - Per group: ~1



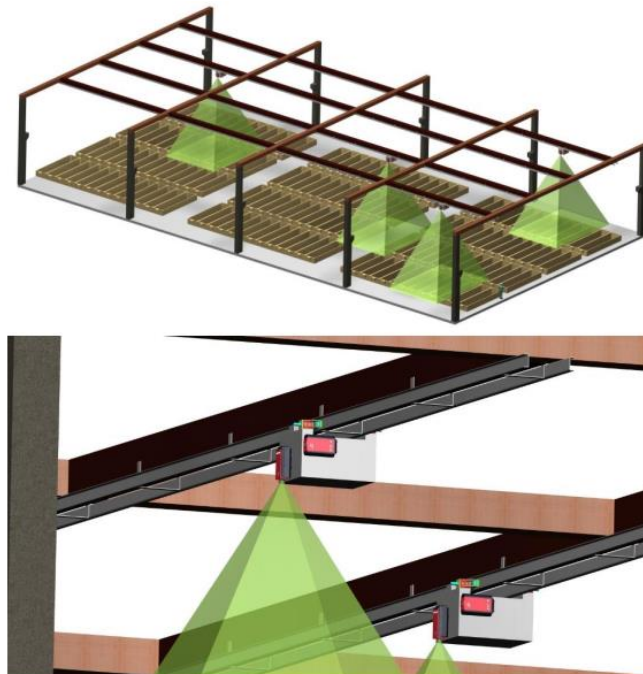
Crane

- Break times for crane are needed
- Monitoring only when crane in “scan mode”
- Small installation effort
- Crane positioning system not needed
- Cameras needed:
 - Per line: 1



Sliding rail

- Semi-Permanent monitoring
 - Independent of the crane
 - Higher installation effort
- Cameras needed:
 - Per line: 1

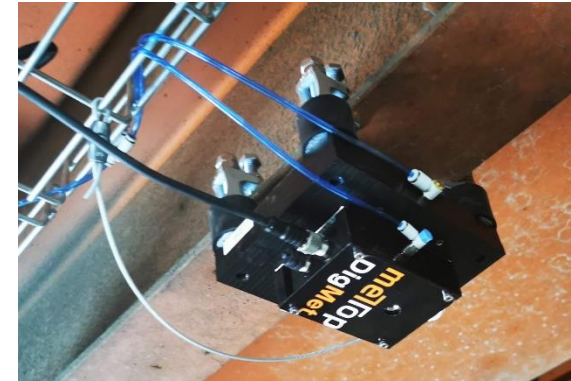


Must be clarified

- Mounting options
- Hall dimensions
- Crane positions
- Crane specification
- Network infrastructure

Study

- 30 days test with one or more fixed cameras
- Report of occurring short-circuits and time
- Self installation on beam on the roof of the hall
- Online-Support
- Test system incl.:
 - 1x Thermal camera incl. cooling solutions
 - 1x Evaluation computer
 - Network components



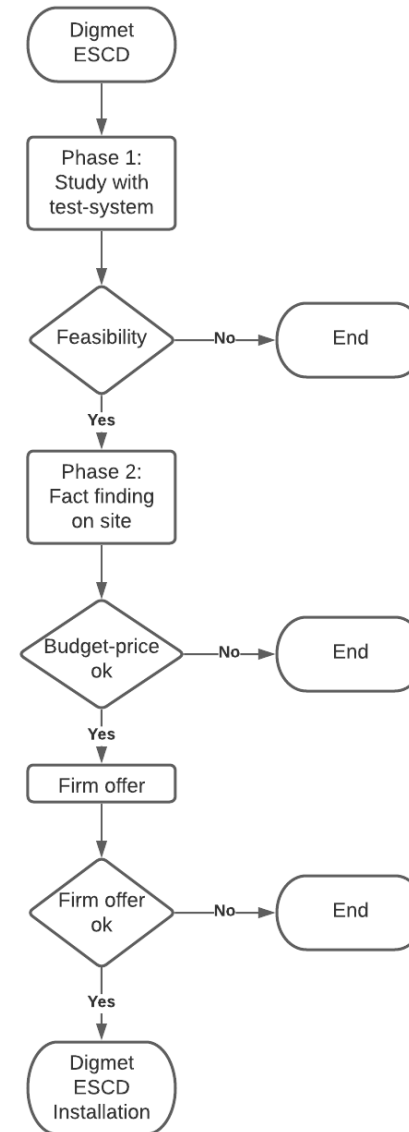
Phases

Phase 1: Study with test system, online support and report

Phase 2: Fact finding on site, defining mounting option and budget price

Phase 3: Firm offer

Phase 4: Installation of ESCD





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